

Title: "Fluid bed granulation process"

DESCRIPTION

Field of application

In its most general aspect, the present invention refers to  
5 a fluid bed granulation process of a suitable substance  
like, for (not limiting) example, urea, ammonium nitrate,  
ammonium chloride and similar substances susceptible to  
being granulated.

More specifically, this invention concerns a fluid bed  
10 granulation process in which the obtainment of granules of  
a predetermined substance occurs through continuous growth  
(of volume and of mass), of granule seeds of such a  
substance, fed continuously into said fluid bed, at the  
same time with a flow of an appropriate growth substance in  
15 liquid state.

In the rest of the description and in the subsequent  
claims, with the terms "granule seeds of a predetermined  
substance", we intend to indicate particles of the  
substance to be granulated, having a size of up to about  
20 2.5 mm. Moreover, for the sake of simplification, we shall  
just use the term "seeds" to indicate granule seeds.

The invention also refers to a granulation apparatus that  
can be used to carry out the aforementioned process.

Prior art

25 It is known that in a fluid bed granulation process of a  
predetermined substance it is necessary to feed seeds of a  
substance to be granulated into said bed and grow them  
through the feeding of a suitable growth substance,

generally the same substance of the seeds, in liquid state, possibly comprising a solvent. In the rest of the description and in the subsequent claims, the predetermined growth substance in liquid state shall also be called 5 growth liquid.

It is known that to reach a good granulation result (predetermined size, shape and mass of the granule) through a fluid bed process of the aforementioned type, it is necessary to ensure a good "wetting" of the seeds and of 10 the granules by the growth liquid.

For such a purpose, it is necessary for the growth liquid to be fed into the fluid bed, in the form of drops that are as small as possible, certainly smaller than the seeds and the granules that are growing with which they are intended 15 to come into contact.

For example, in the case in which the substance to be granulated is urea, this allows the evaporation of the water present in the growth liquid (urea in solution), so as to obtain a finished product (urea granules) with high 20 purity.

In general, the size of the drops of growth liquid is decisive to allow the evaporation of the solvent possibly present in it.

At worst, it is necessary and good that said growth liquid 25 is fed in so-called "atomized" form. In this condition, indeed, the growth liquid manages to meet all of the seeds and granules of substance suspended in the fluid bed individually, to wet them, covering their entire surface uniformly and optimally.

To atomize the growth liquid, the prior art makes use of special nozzles fed with said liquid and large volumes of air (or another appropriate gas) at high speed, for example between 150 and 300 m/s.

5 With wetting complete, the seeds and the granules in growth are subjected to an evaporation step of the possible solvent and then a solidification/consolidation step.

A process of this type, for the production of urea, is for example described in US-A-4 353 730.

10 Although they are advantageous from various points of view, fluid bed granulation processes of the prior art suffer from recognized drawbacks, including the substantial impossibility of controlling the particle size of the finished product within a predetermined range of values and 15 the high operating costs. Indeed, the atomization of said growth fluid is generally obtained with large amounts of high-speed air and this notoriously prevents an adequate, satisfactory control of the growth of the granules inside the fluid bed.

20 Moreover, as a consequence of the aforementioned drawback, it is necessary to make use of classification and screening operations of the granules produced, to take care of the discarding, always considerable, of the granules of unacceptable size (either too big or too small), and of 25 recovery operations of such discard and its recycling upstream of the granulation process.

Other recognized drawbacks of fluid bed granulation processes of the prior art consist of the non-optimal uniform wetting of the seeds and of the granules of 30 substance in growth, as well as the undesired formation of

clots, with the consequent considerable reduction in yield of the entire process.

Summary of the invention

The problem underlying the present invention is that of 5 devising and providing a fluid bed granulation process having functional characteristics so as to overcome all the cited drawbacks with reference to the prior art, i.e. which allows a tighter control of the granulation steps, a substantial reduction in the formation of powders and clots 10 and, last but not least, a considerable improved cost-effectiveness of the process.

The aforementioned technical problem is solved, according to the present invention, by a fluid bed granulation process of a predetermined substance comprising the steps 15 of:

- forming, through a fluidification air flow of predetermined flow rate, a fluid bed of granules of said substance to be granulated, fed to it in form of seeds,
- feeding said fluid bed with a continuous flow of a 20 growth substance (or liquid),

characterized in that it comprises the steps of:

- inducing the formation of a circulatory movement, substantially vortex-shaped, of said granules of the substance to be granulated in said fluid bed and through at 25 least part of said fluidification air flow, and
- maintaining and regulating said circulatory movement through said part of the fluidification air flow.

Advantageously, said fluidification air flow is divided into a plurality of fractions having respective flow rates between a minimum value flow rate, sufficient to support the fluid bed, fed at a first zone thereof and a maximum 5 value flow rate, fed in another zone of the bed itself, so as to induce and maintain said circulatory movement, substantially vortex-shaped, of the granules of said substance.

Further characteristics and the advantages of the invention 10 will become clearer from the detailed description of an embodiment of a granulation process according to the invention, given hereafter with reference to the attached drawings, supplied only for indicative and non-limiting purposes.

15 Brief description of the drawings

Figs. 1 and 2 schematically represent a longitudinal section and a cross section, respectively, of an apparatus (granulator) for carrying out the granulation process of the present invention;

20 Figs. 3 and 3a schematically represent respective plan views of variant embodiments of a detail of the granulator of figures 1 and 2;

Fig. 4 schematically represents a plan view of a variant embodiment of the detail of figures 3, 3a;

25 Figs. 5 and 5a schematically represent a plan view and cross section, respectively, of a further variant embodiment of the detail of figs. 3, 3a;

Fig. 5b represents a cross section of a variant embodiment of the detail of figures 5, 5a;

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Fig. 6 represents the same granulator of fig. 2 for carrying out a variant of the granulation process of the present invention;

Fig. 7 schematically represents a further variant 5 embodiment of the detail of figures 3, 3a.

Detailed description

With reference to figures 1, 2, 3, 3a an apparatus for carrying out a fluid bed granulation process according to the present invention is globally indicated with 1, an 10 apparatus that in the rest of the description shall be more simply called granulator.

In an entirely schematic way, said granulator 1 comprises a container 2, represented open at the top, that is substantially parallelepiped in shape, with a rectangular 15 section.

Said container 2 has a bottom 3, permeable to gas, consisting of a perforated element (grid), two opposite long side walls 4, 5 and two opposite short walls, front 6 or head and rear 7.

20 At the upper side of the head wall 6 a device, schematized as 9, per se conventional and therefore not described in detail, is supported for supplying a continuous flow of seeds S1 of substance to be granulated into the container 2. In the rear wall 7 and at a predetermined height over 25 the bottom or grid 3, an opening 8 is formed, for the discharge, substantially by weir, of the finished (granulated) product from said container 2, as shall become clear in the rest of the description.

In a position below the container 2, a blowing system is provided (not represented since it is totally conventional) of air A or another gaseous fluid (fluidification air), used for carrying out and maintaining a fluid bed of the 5 substance to be granulated inside the container 2.

In accordance with a characteristic of the present invention, the grid 3, which, as stated, constitutes the bottom of said container 2, is essentially a perforated plate (figs. 3, 3a), in which the holes 11, provided for 10 the injection into said container 2 of a predetermined flow rate of fluidification air, are distributed in a non-homogeneous manner.

According to a first preferred embodiment of the invention (fig. 3), all the holes 11 have the same diameter and their 15 distribution in the grid 3 is selected so that their "density", understood as the amount of holes per square centimeter of surface, increases starting from a long wall of the container 2, for example from the wall 4, towards the opposite long wall, for example towards the wall 5. In 20 particular (fig. 3a), according to a further embodiment, said "non-homogeneous" distribution is obtained by defining parallel bands 3a, 3b, 3c, of predetermined width, in the grid 3, in each of which the respective holes 11 are regularly distributed according to a predetermined "pitch" 25 that is different from band to band.

Near to the upper side of the long side wall of said container 2 (in the example the wall 5), adjacent to the zone 3c of the grid 3 of figure 3a, where there is the greatest density of holes 11, a distributor-supplier 10 is 30 supported with conventional means that are not represented, for feeding continuously into said container 2 a flow L of

a predetermined growth substance for granules, for example in the atomized liquid state.

Said distributor 10 substantially extends for the whole length of the wall 5 and at a height over the bottom (grid) 3 which is predetermined according to the thickness of the fluid bed that, as shall become clear in the rest of the description, one intends to carry out in said container 2. Moreover, said distributor 10 is positioned so as to supply a continuous flow of growth substance orientated, in the 10 example described here, substantially parallelly to said grid 3.

With reference to the granulator 1, schematically described above (figures 1 to 3a), an exemplifying embodiment of the granulation process of the present invention shall now be 15 illustrated.

In an initial condition, a fluid bed of seeds S1 of the predetermined substance to be granulated is carried out in the container 2, with a totally conventional technique, said seeds being fed continuously at the head wall 6 of the 20 container itself, through the distributor 9. Such a fluid bed is obtained, supported and maintained through a suitable continuous air flow A (fluidification air), of predetermined flow rate, fed from below and continuously into the container 2, through the grid 3 thereof. When the 25 thickness of the fluid bed, continuously fed with seeds S1, is such that its free surface reaches the level of the opening 8, a continuous "discharge", substantially by weir, of the finished granules out from the container 2 begins.

The fluidification air A, crossing the bottom 3, is 30 distributed inside the bed in a "non-homogeneous" manner,

corresponding to the "non-homogeneous" distribution of the holes 11, provided on said bottom (grid) 3. Where the density of the holes 11 is greater, there is a greater passage of air; in the exemplified case (figure 3a), a 5 greater flow rate of fluidification air A is obtained in the band 3c of said grid 3, near to the wall 5, and a lower flow rate of fluidification air A is obtained in the band 3a near to the opposite wall 4.

Now, the flow rate of fluidification air, its speed, the 10 diameter of the holes 11 and their "density" in the different bands or zones of the grid 3 are selected so that the formation and support of the fluid bed is ensured at the band(s) or zone(s) of lower density. Consequently, due to the structure of the grid of the present invention, at 15 the other bands of said grid and, in the exemplified case, as one approaches the wall 5 of said container 2, the increasing values of flow rate and speed of the fluidification air determine a dragging upwards, towards the free surface of the fluid bed, of the granules in 20 growth. The degree of such dragging also increases as one approaches said wall 5, at which it reaches its maximum value.

As a first effect, this increase in the degree of dragging upwards, applied on the granules of the fluid bed, 25 determines the formation, in the fluid bed, of a circulatory movement, substantially vortex-shaped V, of the granules around an ideal axis which, in the example of figures 1 and 2, is substantially horizontal, said circulatory movement extending helically from the front 30 wall 6 to the rear wall 7 of said container 2.

Basically, with the use of a container 2 having its bottom or grid 3 structured in the way described above, the granulation process of the present invention essentially consists of distributing the flow rate of fluidification 5 air in the fluid bed, carried out in said container 2, dividing it into a plurality of flow rate fractions, having respective values between a minimum amount, sufficient to support said fluid bed and fed at a first zone 3a thereof, and a maximum amount, fed in a zone 3c of said bed, spaced 10 out from said first zone 3a, so as to induce and maintain a circulatory movement of granules, substantially vortex-shaped, in the fluid bed itself. It should be noted that in the exemplified case, the variation in fluidification air 15 flow rates between said first zone where the flow rate is minimum and the zone spaced out from it where the flow rate is maximum, is of the steps type. In the case of figure 3, instead, the fluidification air flow rates vary, between the zone near to the side wall 4 where the flow rate is minimum and the zone near to the side wall 5 where the flow 20 rate is maximum, in a gradual and continuous manner.

As a second effect, the aforementioned dragging upwards determines, within said circulatory movement and, more specifically, in the ascending tract thereof, a thinning of the granules, a mutual spacing out thereof, which is more 25 evident, indeed, near to the wall 5 of the container 2, in other words at the zone of said grid 3 where the "density" of the holes 11 is greater, in other words where the fluidification air flow rate injected into the fluid is greater.

30 At the greater thinning of the granules and where the temperature of the fluidification air is greater, the wetting of said granules by the growth liquid, fed in

atomized form, takes place. Precisely because they are thinned, in other words well spaced out from each other, the wetting of the granules takes place in a very uniform and optimal manner. Consequently, the uniformity of growth 5 of the granules themselves is improved. Moreover, where the aforementioned wetting of the individual granules takes place, the air of the flow responsible for the rotary stream of granules that has formed in the fluid bed is hot and uniformly and optimally takes care of the evaporation 10 of the possible solvent used in the growth liquid. Consequently, the thickness of the "new" layer of growth substance deposited on every single granule is uniform and optimal.

After wetting, the individual granules move towards the 15 opposite wall 4 of the container 2, together with the granules that immediately follow them in the aforementioned circulatory movement, thus running through successive zones of the fluid bed in correspondence of which the grid 3 has bands 3b, 3a, with gradually reducing density of holes 11. 20 In these zones of the fluid bed the upward thrust applied by the fluidification air, which is maximum near to the wall 5 of said container 2, decreases down to zero. For such a reason, near to said wall 4, the stream of the granules naturally deviates towards the bottom or grid 3 of 25 the container 2.

In the course towards the bottom 3, the individual granules of said circulatory movement cross underlying layers of the fluid bed, which are gradually cooler. During this course the solidification/consolidation step of the growth liquid 30 is carried out on the surface of every single granule, a step that is completed during the subsequent tract extending up to the wall 5 with the obtainment of

respective granules having slightly increased volume and mass. From here every single granule begins a new growth cycle that is the same as the one described above, whilst it also moves towards the discharge wall (helical movement 5 of the "vortex").

In accordance with this embodiment of the invention, the granules produced are polydispersed, in terms of particle size, in a very limited range, with respect to that which has been possible up to now with fluid bed granulation 10 processes according to the prior art.

This is advantageously made possible thanks to the fact, quoted above, that every single granule of substance is subjected to substantially the same growth process, since the operating time of each cycle (wetting, drying, 15 desiccation and solidification) and the number of cycles to be carried out inside the fluid bed can be controlled, controlling the variations in flow rate of the fluidification air flow in the different zones of said fluid bed.

20 Moreover, thanks to the granulation process according to the present invention, there is a substantial reduction in the formation of powders, with respect to the processes according to the prior art. This means a reduction, if not even an elimination, of the apparatuses necessary for the 25 recovery of such powders which, together with the possibility of obtaining a finished product of suitable particle size, i.e. directly "sellable", allow the investment and maintenance costs, as well as the energy consumption, of the relative granulation plant to be 30 considerably reduced.

Last but not least, the use of the fluidification air to induce and maintain the aforementioned circulatory vortex movement in the fluid bed of granules in growth, advantageously allows the use of additional external energy 5 sources to achieve the same purpose to be avoided and consequently reflects positively on the efficiency of the process, decreasing consumption.

According to an alternative embodiment (fig. 4) of the present invention, the distribution of the holes 11 in the 10 grid 3 is uniform, but the holes themselves have different diameters. In particular, the diameter of the holes gradually increases as one approaches the wall 5 on which the distributor-supplier 10 is supported; i.e. there are large holes near to the wall 5 and progressively smaller 15 holes as one approaches the wall 4. In this case the variation of fluidification air flow rates is gradual and varies between the zone where it is minimum and that where it is maximum, in the same way as the embodiment of figure 3.

20 According to a further embodiment of the invention, the formation and the maintenance of the circulatory vortex movement of the granules, described above, are obtained not by dividing the fluidification air flow into a plurality of portions of different flow rate, but by suitably varying 25 the entry direction of such a flow into the fluid bed.

For such a purpose, for example (figures 5, 5a), the holes 11 of the grid 3 are uniformly distributed, they all have the same diameter, and they are all equally inclined on the horizontal by a predetermined angle  $\alpha$ , preferably between 30 30° and 60°, for example 45°.

The inclination of said holes is selected in such a way that the thrust of the air on the granules has a vertical component such as to ensure the support of the fluid bed and a horizontal component that allows the creation and 5 maintenance of the rotary motion of the granules in the fluid bed.

As an alternative to this embodiment, the holes 11 of the grid 3 are uniformly distributed, they all have the same diameter and are vertical; the grid 3 is equipped with 10 deflectors 20 (fig. 5b) consisting of metallic foils inclined towards the wall 5 of the container 2 by a predetermined angle  $\alpha$  to the horizontal preferably between 30° and 60°, for example 45°, associated with, preferably welded to, said grid 3 at the holes 11 and with a 15 predetermined distance from the holes 11.

In this way, the fluidification air coming out from the holes 11 is directed, in the same way as the embodiment represented in figure 5a, in such a way as to allow the formation of the aforementioned rotary stream of granules 20 inside the fluid bed. With reference to figure 6, a further advantageous variant embodiment of the granulation process of the present invention provides the formation of two opposite circulatory movements of granules, V1 and V2, in the same fluid bed of the substance to be granulated.

25 For such a purpose, the container 2 is equipped, on both of the opposite long side walls 4, 5, with respective distributors 10a, 10b for supplying flows L, L1, of the same growth liquid and with a grid 3, with through holes 11, arranged according to symmetrically opposite and equal 30 distributions, with respect to a middle axis M-M. In such a figure 6, the details of the granulator 1 that are

structurally and functionally equivalent to those illustrated in the previous figures are indicated with the same reference numerals. In particular, the through holes 11 of the grid 3 are of the type described with reference 5 to figures 3-5b.

Thanks to this embodiment it is possible to double the production capacity of the granulator intended to carry out the granulation process according to the invention, keeping the operating conditions of the fluid bed constant.

- 10 In accordance with a further variant embodiment of the granulator 1 of the present invention, the seeds S1 and the flow L1, L2 comprising the growth liquid are fed into said fluid bed in correspondence of at least one same side wall 4, 5 of the container 2.
- 15 Such a container 2 has a bottom or grid 3 (fig. 7) equipped with holes 11 distributed, in two symmetrically opposite zones, in the same way as the one described with reference to the previous embodiment illustrated in figure 4; said bottom is also equipped with a plurality of slits 14, for 20 discharging granules, of a suitable size and with a width correlated with (greater than) the diameter of the granules intended to be produced. It goes without saying that the present embodiment of the invention can also be used with the other embodiments of the invention, relative to figures 25 3-3a and 5-5b.

The discharge of the finished granules from the bottom 3 of the container 2 occurs by gravity, preferably in countercurrent to a flow A of air or another suitable classification gas fed into said fluid bed through said

slits 14. According to this embodiment, the rear wall 7 is, of course, without the opening 8.

The invention thus conceived is susceptible to further variants and modifications all of which are within the 5 scope of protection of the invention itself, as defined by the following claims.